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A Novel Pretreatment Process for Direct Electrodeposition onto Aluminum Alloys

by

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ABSTRACT

This paper will discuss a novel pretreatment process for direct electrodeposition nickel-phosphorus (NiP) and nickel (Ni) from commercial electrolytes onto aluminum (Al) alloy (T6061) surfaces without the need for zincate or stannate pretreatment processes. We will compare these coatings properties to conventional commercially applied electroless (NiP) using conventional pretreatment processes.

Introduction

The direct electrodeposition of coatings onto Al and its alloys is difficult due to the formation of a strongly adherent passivating oxide film. Over the past 50 years there have been numerous publications on the subject,¹⁻⁷ each addressing the challenge of removing this passive oxide film such that the coating could be directly applied to the Al substrate. If this passive oxide is not properly removed, the applied coating exhibits poor adhesion, corrosion resistance, solderability or other critical performance properties.

In a general sense, the most common pretreatment approaches for oxide removal involves using either zincate or stannate immersion coating processes in which the surface Al reacts with either the soluble Zn or Sn ions to deposit Zn/Sn.² Once the Zn or Sn coatings are applied, they may be directly removed within a strip or through replacement within electroless Cu or NiP chemistries to produce a Cu or NiP deposit on the Al substrate.

A conventional Al pretreatment process is shown in Fig. 1. The processing line consists of etching, desmutting, zincating and electroless nickel phosphorus tanks that will require consistent tracking and maintenance.⁸⁻¹² The floor space requirements are considerable, with approximately sixteen processing tanks. Depending on the size of the parts, the tanks range in volume from 50 to 500 gallons. The rinse water tanks require regular water recovery and waste treatment cycles. Additional safety considerations are required due to the presence of HF.

Such an extensive number of processing steps and tanks requires significant capital investment for a new vendor, increases the probability of errors during the process, is time consuming (lower industrial throughput that ties up equipment) and requires large volumes of hazardous chemicals that are environmentally unfavorable and introduce cost and safety concerns. Therefore, alternative coating techniques are needed that do not require such extensive pretreatment processing with similar or better performance to conventional electroless NiP. Herein, we present a novel, single-step pretreatment process using an environmentally benign solution pretreatment approach without zincate or stannate pre-processing steps (Fig. 2). We report the material properties of Ni and/or NiP coatings directly electrodeposited onto to aluminum alloy substrates (T6061).

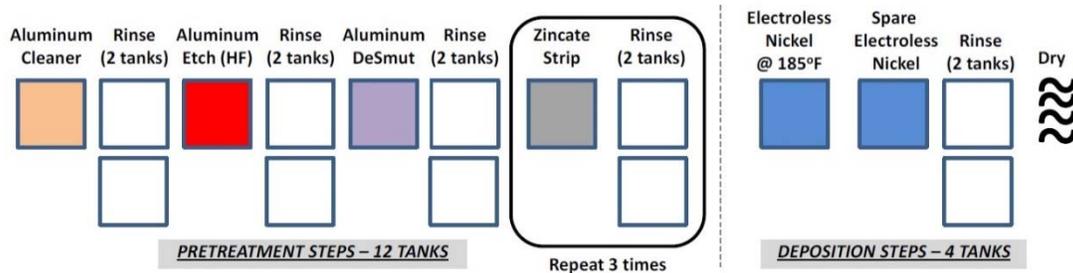


Figure 1 - Conventional electroless NiP on aluminum alloy T6061.

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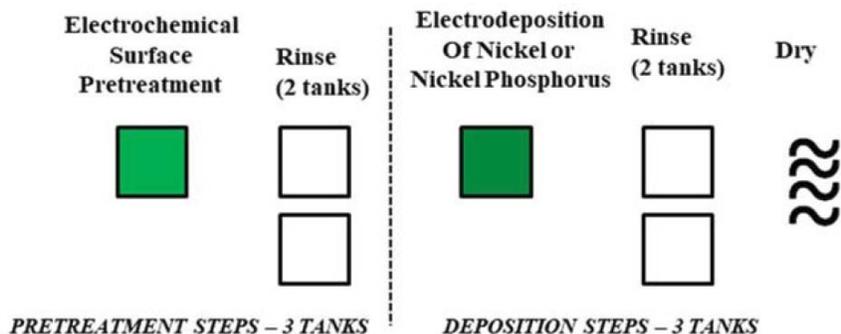
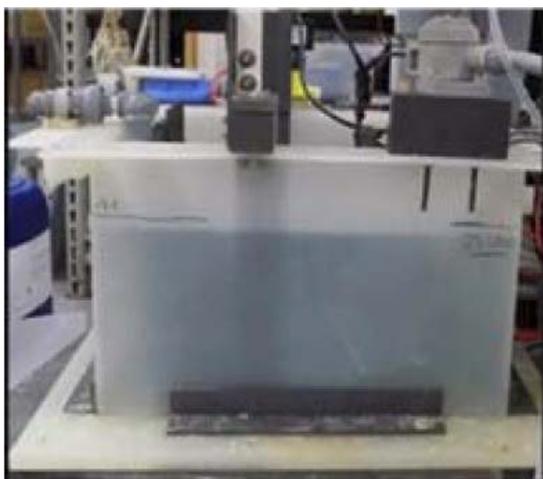


Figure 2 - Scalable five-step, environmentally-friendly electrochemical pretreatment and electrodeposition process.

Experimental

Construction of electrochemical tooling for electropretreatment and deposition

Bench-scale tooling was designed and built to enable aluminum pretreatment and direct deposition of nickel (Ni; Watts Ni), or nickel-phosphorus (NiP; Umicore NIPHOS® 968) onto Al alloy (T6061), as shown in Fig. 3.¹³⁻¹⁵ The complete process system (left to right) includes an electropretreatment tank (A), rinse tank (not shown) and electrodeposition tank (B) for Al (T6061) panels. The electrochemical cell incorporates thermal management (cooling coil/ heat element (not shown)), a pump for electrolyte circulation and a filter. All T6061 aluminum alloy substrates were procured from commercial sources.



(A) Electropretreatment



(B) Electrodeposition

Figure 3 - Images of electropretreatment cell (A) and NiP electrodeposition cell (B)

Pulse-reverse electropretreatment of 6061 aluminum

The patented electropretreatment of the aluminum alloy (T6061) surfaces (U.S. Patent Application number: 16/869,014)¹⁶ was done at a controlled temperature of 50°C using pulse-reverse voltage waveform⁹ in a 10% H₂SO₄ + 100 g/L Na₂SO₄ electrolyte.¹⁷ The electrochemical pretreatment process is done under pulse-reverse voltage control in order to lessen sensitivities to geometric considerations. After electrochemical pretreatment, the coupons were removed from the cell, rinsed with deionized water and transferred to the electrodeposition cell for direct electrodeposition of the targeted coatings. For all electropretreatment activities, the counter electrode used was a mixed metal oxide (MMO) coating on titanium, with an approximate anode-to-cathode gap of 3-4 inches.

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Electrodeposition conditions

Throughout the course of multiple activities, we utilized various commercially available electroplating electrolytes. For direct Ni electrodeposition we prepare a conventional Watts electrolyte (pH 4.0 at 80°F) and deposited it at a current density of 4 A/dm² using a pure Ni anode. For direct NiP electrodeposition, we procured NIPHOS® 968 electrolyte (pH 2.6 at 140°F) from Umicore and electrodeposited it at a current density of 4 A/dm² using a sulfur-activated nickel anode. After electrodeposition, the coupons were removed from the cell, rinsed with deionized water, dried by pressurized air, and photographed.

For comparison to electroplated coatings we contracted Techmetals Inc. (Dayton, OH) to apply a conventional electroless NiP with standard high phosphorus (9-11% P) to the 6061 aluminum alloy.

Physical characterization

The coating uniformity, surface morphology and composition were investigated using a magnetic probe (Elcometer 456), XRF (Bruker, S1 TITAN Handheld) and confirmed with cross sectional analysis (Nanovea ST-400 optical (non-contact) profilometer (Nanovea, Irvine, CA)). Bend-to-break adhesion and microhardness tests were performed by Fermi National Accelerator Laboratory. MIL-A-8625F corrosion testing was done by Metallurgical Solution Inc. (MSI, Middletown, OH). Additionally, the surface finish (roughness (R_a)) before and after processing was evaluated using a contact micrometer probe (Mitutoyo SJ400 Profilometer).

Results and discussion

Pulse-reverse electropretreatment of 6061 aluminum

Figure 4 shows a generalized pulse reverse electrochemical surface pretreatment waveform.¹⁸ The forward (anodic) pulse amplitude and on-time are tuned to partially oxidize the surface such that this oxide can be dissolved within the electrolyte during the reverse (cathodic) pulse amplitude, eliminating the need for hydrofluoric acid to remove the oxide.¹⁹⁻²¹ The off-time (anodic or cathodic) allows for heat dissipation.

Utilizing our patented pulse/pulse reverse electrochemical pretreatment process, we pretreated specified 6061 T6 specimens and performed analysis on the coatings applied using standard operating conditions from the various commercially available electrolytes discussed earlier. One difference between the typical plating processes and the one used here was that, after pretreatment and rinse, a slight cathodic overpotential was applied to the sample to cathodically protect it during introduction to the plating electrolyte.

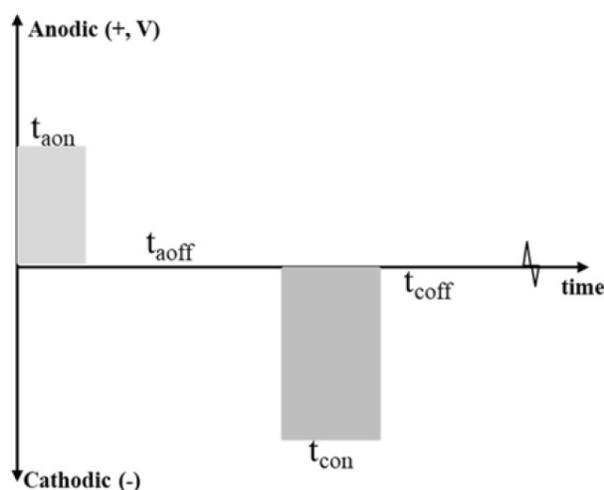
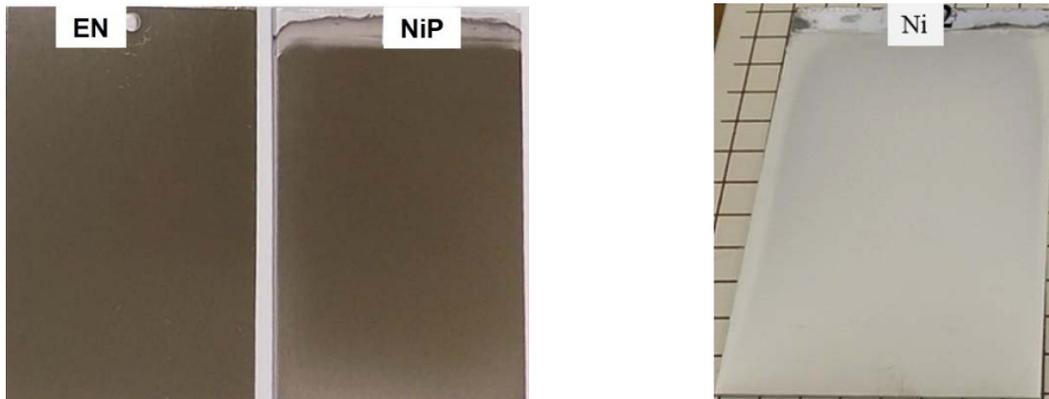


Figure 4 - Generalized pulse reverse electrochemical surface pretreatment waveform.

Coating visual, thickness, surface roughness and microhardness analysis

Figure 5 shows 4" × 6" 6061 Al panels coated with the commercially available deposits. Specifically, we observed that the color difference, hardness, roughness, composition and microstructure between the standard electroless NiP and the electrolytic NiP were nearly identical. When comparing these baseline materials to the nickel deposits, you can clearly see a change in the visual color and hardness, but microstructurally the coating appeared to be well adherent to the substrate.

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As Plated	Thickness, μm	Microhardness HV	Ra, μm	SEM-EDX, wt%	
				Ni	Phosphorus
EN	23	~500*	0.2 ± 0.06	89 ± 0.03	10.7 ± 0.03
NiP	40	501-540	0.3 ± 0.04	88 ± 0.04	10.8 ± 0.04
Ni	12	249	0.3 ± 0.02	100	0

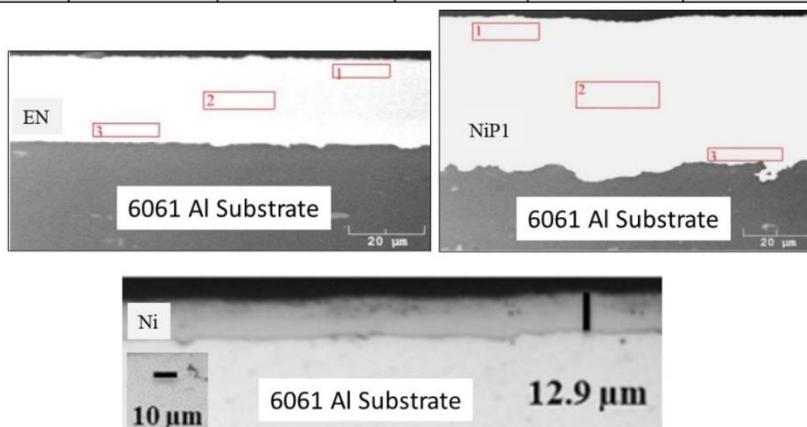


Figure 5 - (Top) Images of electroless NiP, electrolytic NiP and nickel directly applied to 4" x 6" 6061 T6 Al panels; (Middle) Table of measured deposit composition, thickness, roughness and hardness; (Bottom) Representative cross-sections for each coating system on aluminum.

MIL-A-8625F corrosion test

Salt spray testing was performed in accordance with MIL-A-8625F by an accredited facility MSI (Middletown, OH; accredited A2LA). The detailed procedures used by MSI to perform the test were: (1) clean panel surfaces with acetone; (2) install panels in cabinet at -6° from the vertical and parallel to the flow of the fog, in accordance with MIL-A-8625F paragraph 4.5.3.1 (with an exposed area of 15 in²); (3) run the test on all panels to termination (which is 336 hr per MIL-A-8625F); (4) after testing, rinse the panels with running distilled water at less than 100°F; (5) examine the surfaces with an Olympus SZ61 stereoscope with Pax-it image analysis software to look for corrosion and blistering and (6) count the number of pits per ASTM E29 for the NiP and Ni samples.

The coated 6061 panels after the specified salt spray corrosion testing are shown in Fig. 6, while Table 1 shows the results of the post corrosion analysis. The data indicate that both the electroless NiP and DC electrodeposited nickel phosphorus-coated samples passed the corrosion test (MIL-A-8625F paragraph 6.19 and 3.7.1.2) identified over 150 in². However, the nickel-coated samples did not pass the pitting requirements for the test.

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Post 336h salt fog test

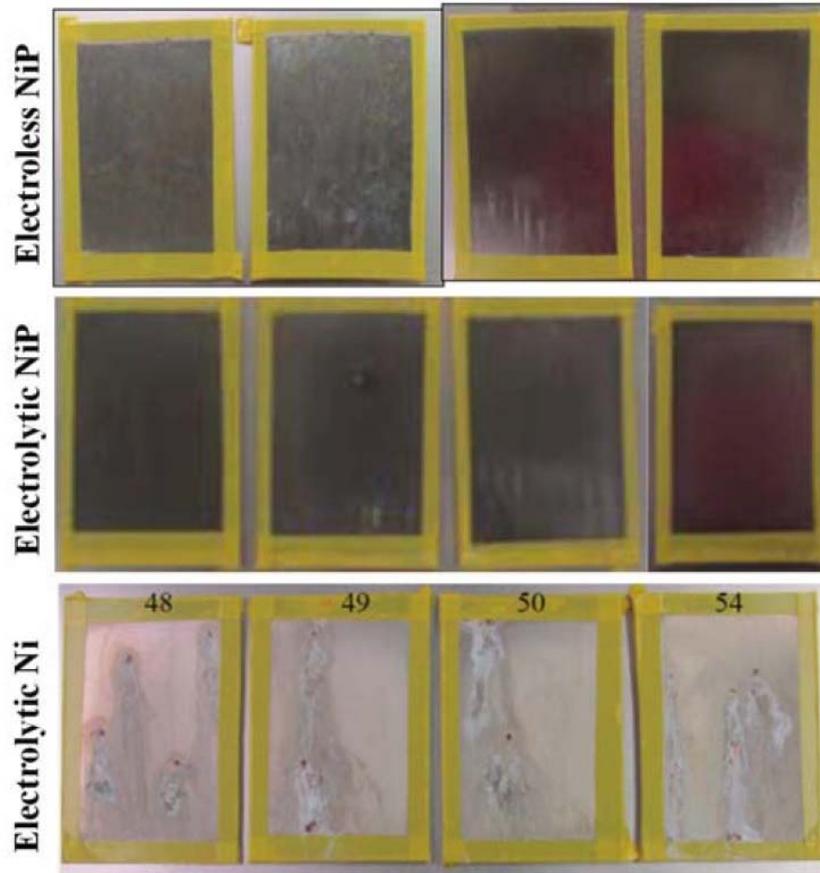


Figure 6 - Surface images of post-salt spray corrosion test electroless NiP, electrolytic NiP and electrolytic Ni applied to 6061 Al.

Table 1 - Analysis of coupons post the MIL-A-8625F corrosion test for coatings on 6061 Al from Fig. 6.

Coupon Type	Coupon Label	Number of Pits	Corrosion Test Time (h)
Electroless NiP	EN7	0	336
	EN8	0	
	EN9	0	
	EN10	0	
Electrolytic NiP	106	0	
	108	0	
	109	0	
	110	0	
Electrolytic Ni	81	6	
	83	3	
	84	0	
	85	5	

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Bend test

The Bend test was performed at Fermilab, by Mr. Cory Crowley. The initial bend tests were done with a 0.5" bend radius on the flat panels, as shown in Fig. 7. Both the electroless nickel phosphorus (EN1, EN2), the electrolytic nickel (16, 17) and the electrolytic nickel phosphorus (96, 102) passed the test and showed good adhesion as depicted in Fig. 7 and Table 2.

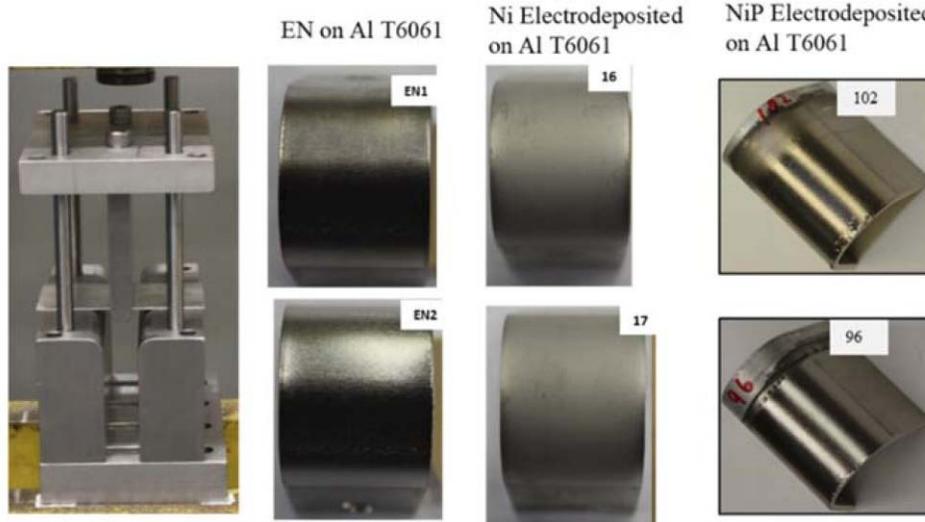


Figure 7 - From left to right is 1) the device for the Bend test; 2) the inflection point of the electroless NiP (EN1, EN2); 3) electrodeposited nickel (16, 17) and electrodeposited nickel phosphorus (96, 102) coupons after the 0.5" bend radius test.

Table 2 - Summary of the bend test (0.5") results

Coupon	Process	Observation
EN1	Electroless Nickel from Techmetal	Pass
EN2		
16	Ni electrodeposition after one step electropretreatment	Pass
17		
96	NiP electrodeposition after one step electropretreatment	Pass
102		

Bend tests were also performed using a 0.25" bend radius on 1" x 4" x 0.1" 6061 Al panels, with the primary goal of achieving adhesion failure of the coating. Both the electroless NiP coupons and electrolytic Ni passed the test, though electrolytic NiP showed adhesion failure on the edges of the coupons, as shown in Fig. 8 and summarized in Table 3. The surface cracking on the edges of the flat electrolytic nickel phosphorus panels is a phenomenon that typically is eliminated when plating actual shaped components, *e.g.*, cylindrical shapes, because most parts are without sharp edges, or high current density regimes.

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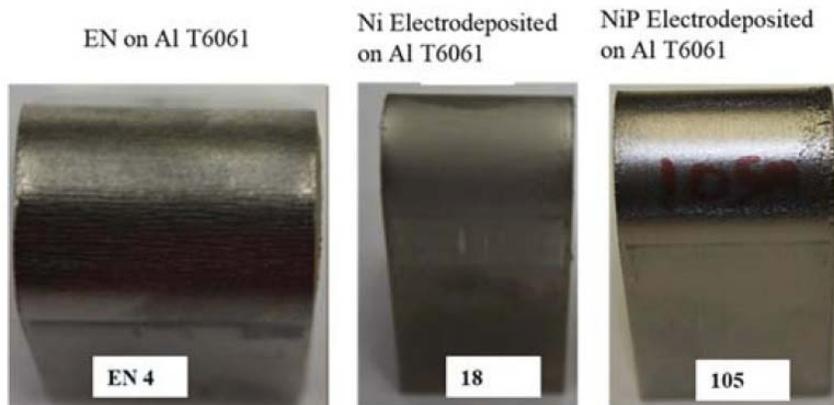


Figure 8 - Left to right: The inflection point of the electroless NiP (EN4), electrolytic Ni (18) and electrolytic NiP (105) coupons after the 0.25" bend radius test.

Table 3 - Summary of the bend test (0.25") results

Coupon	Process	Observation
EN4	Electroless Nickel from Techmetal	Pass
18	Ni electrodeposition after one step electropretreatment	Pass
105	NiP electrodeposition after one step electropretreatment	Coupon edge blister

Wear test

The Taber wear testing was performed at Fermilab using a 5135 Abraser per ASTM D4060. The wear index trials test conditions are as described in Table 4 (Left). The measured Taber wear index number (mass loss/# cycles /1000) measured until coating breakthrough is shown in Table 4, Right. The exemplar coating breakthrough for representative sample tested is shown in Fig. 9, where the aluminum layer that had been broken through has a noticeably whiter appearance as compared to the nickel phosphorus coating. The measured Taber wear index number at runout for each sample tested is very similar except for coupon 102. Overall, since wear is related to the hardness and microstructure of the material in contact with the wheel, this wear index number similarity between ENi and NiP electrodeposited coupons indicates their materialistic similarities.

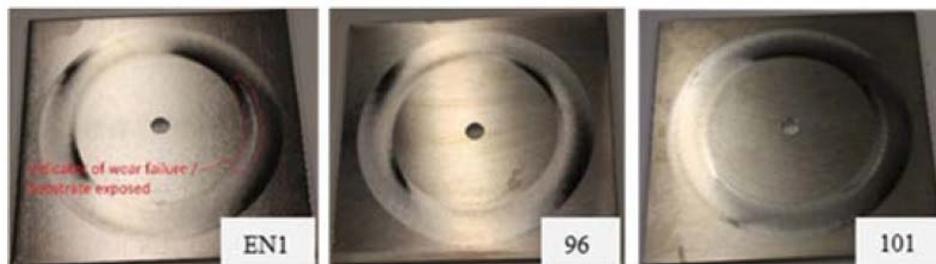


Figure 9 - Images of electroless NiP (EN 1) and representative electrolytic NiP (96, 101) coupons after the taber wear test, undertaken at FermiLab

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Table 4 - Taber wear test conditions (Left) and results for EN and NiP electrodeposited coupons (Right)

Test Date	06/11/2019
Temperature (F)	70.7 °F
Humidity (% RH)	63%
Abrading Counterweight	750 g
Speed Control	60 RPM
Vacuum Power	100%
Abrading Disc Type	CS-10
Recondition Frequency	500 Cycles

Coupon	Process	Wear Index @ Failure Cycles, mg/1000 cycle
EN1	Electroless Nickel	23.6
96	NiP Electrodeposited on Al T6061	22.7
101		23.2

Conclusion

In summary, we have successfully demonstrated the potential of a scalable five-step environmentally-friendly electrochemical pretreatment process that can be utilized to prepare 6061 aluminum alloy for direct electrolytic deposition of nickel and NiP without the need for zincate or stannate pretreat approaches. Reports herein demonstrate similar metallurgical, corrosion and material properties for electrolytic NiP and electrolytic Ni directly applied to Al when compared to electroless NiP coatings prepared through a zincate process. Therefore, this new approach to prepare Al for direct deposition can significantly reduce the number of processing steps, hazardous chemistry use, cost and capital investment. Furthermore, this electrolytic deposition process is much more rapid and less sensitive to chemical changes, enabling better part throughput. Currently, we are continuing to optimize the electropretreatment and electrodeposition process to further improve the coating properties and enable process scalability.

Acknowledgements

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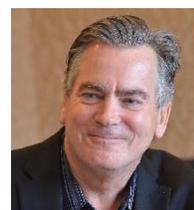
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Dr. Maria Inman is the Research Director at Faraday. Dr. Inman leads Faraday's research and development function. In addition to providing day to day direction to the science and engineering staff at Faraday, Dr. Inman has served as Principal Investigator on millions of dollars worth of government and commercially-funded projects and serves as an integral member of Faraday's internal strategic planning and IP management group. Dr. Inman has been on staff at Faraday for 26 of its 30 years in business.



Dr. E. Jennings Taylor uniquely blends 40+ years entrepreneurial business experience with demonstrated skills in technology innovation and intellectual asset analysis. Prior to forming Faraday, Dr. Taylor held positions at Giner, Inc. as the Manager of Fuel Cell Research (1982-1985), and at Physical Sciences where he held numerous positions including the Manager of Electrochemical Technologies (1985-1991). In 1991, EJ left Boston to form Faraday Technology, Inc. He successfully secured start-up funding and from 1991-1997 served as the Principal Investigator on many of Faraday's early research projects. In 1997, Dr. Taylor shifted his emphasis from research to strategic corporate direction and technology portfolio management. In order to facilitate the development of an intellectual property portfolio, he studied to become a Patent Agent and in February, 2003 was granted the status of registered agent with the US Patent and Trademark Office. Dr. Taylor applies this skill to develop patent portfolios that can benefit potential customers. EJ is well recognized in both the professional and business community. He is co-chair of the Technical Advisory Committee for SURFIN/NASF, Chair of the NASF/AESF Foundation Research Board, a past Treasurer of the Electrochemical Society, and a past Chair of the SBIR Advisory Board of the National Science Foundation.